Ammonia–Phosphoric Acid–Water System at 25° C. Density, Viscosity, pH, Conductance, Vapor Pressure

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 $P_{HYSICOCHEMICAL}$ data on aqueous phosphate systems (10, 17) are extended here by information on the density, viscosity, pH, electrical conductance, and partial pressures of water and ammonia of solutions in the system ammonia-phosphoric acid-water at 25° C.

Solubilities in the system are reported fully in the literature (5, 11, 14, 15, 19). Data on vapor pressures (6, 9, 16), pH (1), and conductances (21) of the solutions are few, although vapor pressures (8), densities (3), and viscosities (7) of phosphoric acid solutions are reported.

The present study covers solutions containing up to 50% H₃PO₄ and having mole ratios NH₃:H₃PO₄ up to 11.5.

PREPARATION OF SOLUTIONS

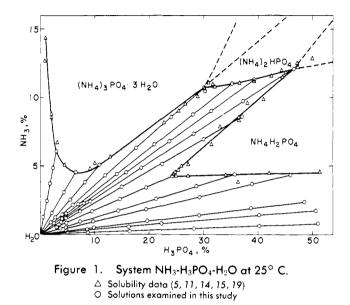
Most of the solutions were prepared from reagent grades of phosphoric acid and ammonium hydroxide, a laboratory preparation of monoammonium phosphate (from cylinder ammonia and reagent-grade phosphoric acid), and distilled water. Saturated solutions at various mole ratios $NH_3:H_3PO_4$ above 0.5 and solutions containing 50% H_3PO_4 at mole ratios $NH_3:H_3PO_4$ of 0.1, 0.2, and 0.3 were diluted with distilled water to traverse the line between the concentrated solution and the water corner.

Most of the solutions were analyzed precisely for ammonia and phosphorus, but some of the more dilute solutions were prepared by weight dilution of more concentrated solutions with conductance water. All the solutions with mole ratios $NH_3:H_3PO_4$ of 0.1 and 0.2 (used only for determinations of conductance, density, and pH) were prepared with conductance water. The compositions of the solutions in the present study are superimposed in Figure 1 upon a plot of the solubility isotherm at 25° C. as derived from published data (5, 11, 14, 15, 19).

MEASUREMENTS

Density. Density was measured with 25-ml. pycnometers of the modified Gay-Lussac type.

Viscosity. Viscosity was measured with Cannon-Fenske



routine viscometers that were calibrated with water as the primary standard. The viscosity of water at 25° C. was calculated (4) to be 0.8902 centipoise from the reliable value at 20° C. (18).

pH. pH was measured with a glass electrode in a portable pH meter (Leeds & Northrup, Model 7661).

Conductance. Electrical conductance was measured with the equipment and by the methods of Mason and Culvern (13). Readings were corrected for calibration of the electrical bridge. The cells were standardized with solutions of potassium chloride, thrice crystallized from water and fused (12). The temperature of the oil bath was measured with a Beckman thermometer which was checked against a platinum resistance thermometer calibrated by the National Bureau of Standards.

Table I. Density, Viscosity, pH, Conductance, and Vapor Pressure

Mole								Conductance		Partial Pressure, Mm. Hg.	
Ratio	Compn., %		Molality		Density,		Viscosity,	Specific,	Molar,		
NH ₃ :H ₃ PO ₄	NH3	H ₁ PO ₄	NH ₃	H ₃ PO ₄	Grams/Ml.	pН	Cps.	ohm ⁻¹ cm. ⁻¹	ohm	NH	H_2O
11.54	6.09	3.02	3.93	0.34	1.0009	10.54	1.092	0.031361	101.6760	50.541	22.519
	4.84	2.42	3.07	0.27	1.0000	10.42	1.046	0.027574	111.6633	38.428	22.956
	3.65	1.82	2.27	0.20	0.9993	10.37	1.005	0.023039	124.3920	27.177	23.211
	2.43	1.22	1.43	0.12	0.9987	10.30	0.964	0.017356	139.5985	16.995	23.484
	1.22	0.61	0.73	0.06	0.9984	10.18	0.927	0.010395	167.2693	7.260	23.643
3.97	4.53	6.60	2.99	0.76	1.0432	10.00	1.246	0.059891	85.2464	24.237	23.011
	3.04	4.40	1.93	0.49	1.0281	9.89	1.101	0.046709	101.1902	14.389	23.155
	1.52	2.20	0.93	0.23	1.0127	9.78	0.987	0.028656	126.0486	6.443	23.542
2.69	5.08	10.91	3.55	1.33	1.0839	9.62	1.547	0.084025	69.6339	15.632	22.765
	3.80	8.15	2.53	0.95	1.0620	9.58	1.312	0.072270	81.8280	10.408	23.010
	2.55	5.44	1.63	0.60	1.0406	9.50	1.138	0.056040	97.0164	6.270	23.353
	1.28	2.72	0.78	0.29	1.0191	9.40	1.002	0.034181	120.8440	2.857	23.543
	0.86	1.83	0.52	0.19	1.0120	9.17		0.025233	133.5224	• • •	• • • •
2.05	10.72	30.02	10.62	5.17	1.2465	8.70	6.793	0.096189	25.1912	4.260	21.198
	8.57	24.07	7.47	3.65	1.1964	8.68	3.765	0.110019	37.4405	3.424	21.966
	6.39	17.98	4.96	2.43	1.1460	8.64	2.336	0.109518	52.0880	2.455	22.461
	4.29	12.01	3.01	1.46	1.0969	8.60	1.584	0.093596	69.6263	1.512	22.961
	2.14	6.01	1.37	0.67	1.0475	8.42	1.153	0.061061	95.0520	0.686	23.335
	1.44	4.02	0.89	0.43	1.0311	8.38		0.045875	108.4619		
	0.71	2.00	0.43	0.21	1.0142	8.23		0.026894	129.9355		

Table I. Continued

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	0.034	20.069
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	$0.025 \\ 0.022$	$21.381 \\ 22.271$
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$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	0.013	23.392
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$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	0.016	18.718
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	0.013	20.712
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	0.012	21.913 22.663
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	0.008 0.005	22.663
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$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	0.002	20.921
$\begin{array}{cccccccccccccccccccccccccccccccccccc$		21.813
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$\begin{array}{c ccccccccccccccccccccccccccccccccccc$		21.325
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$\begin{array}{c ccccccccccccccccccccccccccccccccccc$		19.673
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0.91 9.76 0.60 1.12 1.0562 1.83 1.176 0.046928 44.612 0.45 4.85 0.28 0.52 1.0261 2.05 0.026243 51.678 0.15 1.63 0.09 0.17 1.0069 2.23 0.011071 66.107 0.28 2.35 48.56 2.81 10.09 1.3266 0.00 5.729 0.166685 25.357		21.914
0.45 4.85 0.28 0.52 1.0261 2.05 0.026243 51.678 0.15 1.63 0.09 0.17 1.0069 2.23 0.011071 66.107 0.28 2.35 48.56 2.81 10.09 1.3266 0.00 5.729 0.166685 25.357		22.646
0.15 1.63 0.09 0.17 1.0069 2.23 0.011071 66.107 0.28 2.35 48.56 2.81 10.09 1.3266 0.00 5.729 0.166685 25.357		23.243
0.28 2.35 48.56 2.81 10.09 1.3266 0.00 5.729 0.166685 25.357		• • •
1.87 38.81 1.85 6.68 1.2486 0.38 3.527 0.157228 31.797		18.546 20.484
1.41 29.12 1.19 4.28 1.1781 0.72 2.295 0.127009 36.281		21.782
0.94 19.44 0.69° 2.49 1.1131 1.00 1.587 0.086248 39.061		22.638
0.47 9.75 0.31 1.11 1.0534 1.30 1.159 0.044840 42.785		23.328
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0.55 16.25 0.39 1.99 1.0918 0.96 0.075957 41.956		• • •
0.29 8.65 0.19 0.97 1.0463 1.14 0.041871 45.338		
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0.62 40.36 0.62 6.98 1.2575 < 0 0.198398 38.308 0.44 28.10 0.36 4.01 1.1677 0.29 0.149659 44.698		•••
0.26 16.42 0.18 2.01 1.0923 0.52 0.086657 47.349		
0.13 8.61 0.08 0.96 1.0460 0.95 0.046822 50.949		•••
$\begin{array}{cccccccccccccccccccccccccccccccccccc$		
0.033 2.09 0.02 0.22 1.0087 1.43 0.015605 72.540	•••	

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Vapor Pressure. Partial pressures of water and ammonia were measured by a dynamic method (2). The glass saturator was packed with glass helices. With the more viscous solutions, rates of oscillation of the saturator were as low as two per minute. With solutions that had appreciable pressures of ammonia, a presaturator prevented significant change in the composition of the solution during a measurement.

The two storage bulbs in the displacement meter held 6 liters each. Dried, carbon dioxide-free nitrogen from the bulbs was passed through the saturator at a rate of about 100 cc. per minute; four bulbfuls of gas were used in each determination.

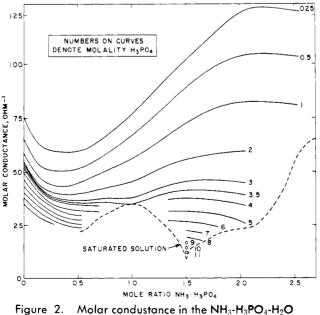
The gas from the saturator was passed through U-tube absorbers, each containing about 3 grams of anhydrous magnesium perchlorate. Two bulbs in series were used in most of the runs—three when the amount of ammonia was large. The tubes were weighed before and after each run, the absorbent was dissolved in water made slightly acidic with sulfuric acid, and the ammonia was determined precisely. Water vapor was determined by difference.

RESULTS

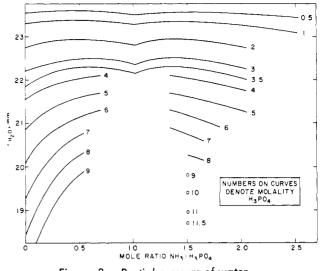
In correlating the results (Table I) molar conductances were calculated on the basis of the phosphoric acid content. Plots of molar conductance against mole ratio NH₃:H₃PO₄ at constant molalities of phosphoric acid (Figure 2) show a dip in the conductance at a mole ratio $NH_3:H_3PO_4$ of 1, which corresponds to monoammonium phosphate. Similar plots of the partial pressure of water (Figure 3) show a similar dip at a mole ratio NH₃:H₃PO₄ of 1. In each series of plots, the dip becomes more pronounced as the concentration is increased to 3.5 molal H_3PO_4 , the concentration corresponding to a saturated solution of monoammonium phosphate.

The partial pressures of water vapor measured in this work are somewhat higher than those reported by Huey and Tartar (9) but are more consistent with the vapor pressures of phosphoric acid solutions reported by Elmore, Mason, and Christensen (8).

The partial pressure of ammonia is very low at mole ratios NH_3 : H_3PO_4 less than 2, which corresponds to diammonium phosphate. The partial pressures of ammonia measured in this work are somewhat lower than those reported by Huey and Tartar (9), although the two sets of results yield curves similar in shape—both in disagreement with Roehl's asser-



system at 25° C.



Partial pressure of water Figure 3.

tion (16), based on Warren's data (20), that the pressure of ammonia over saturated solutions of diammonium phosphate is inappreciable at temperatures below 55° C. As shown in Table I, for example, the partial pressure of ammonia at 25° C. is 4.26 mm. of mercury over a substantially saturated solution 5.17 molal in phosphoric acid and having a mole ratio NH_3 : H_3PO_4 of 2.05.

The results reported in Table I for viscosity, density, and condustance probably are accurate within the limits of error of the analyses of the solutions. The vapor pressure data are less accurate; measurements on the same solution agreed within 0.5% for the partial pressure of water and within 1%for the partial pressure of ammonia at values upward from 1 mm. of mercury.

ACKNOWLEDGMENT

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